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$$\textcircled{1} \quad \frac{p_1 V_1}{p_2 V_2} = \frac{n_1 T_1}{n_2 T_2} \quad p_1 = p_2, \quad n_1 = n_2$$

$$\Rightarrow \frac{V_1}{V_2} = \frac{T_1}{T_2} \quad \Rightarrow \quad V_2 = V_1 \frac{T_2}{T_1}$$

$$T_2 = T_1 + \Delta T \quad \Rightarrow \quad \frac{T_2}{T_1} = \frac{T_1 + \Delta T}{T_1} = 1 + \frac{\Delta T}{T_1}$$

↳ man braucht die absolute Temp., die Differenz allein ( $\Delta T$ ) reicht nicht!

$$\textcircled{2} \quad \frac{E}{V} = \frac{35 \text{ MJ}}{\text{Liter}} \Rightarrow E = 35 \text{ MJ} = 35 \cdot 10^6 \text{ J.}$$
$$\eta = \frac{E_{\text{Nutz.}}}{E_{\text{zugef.}}} \Rightarrow E_{\text{Nutz.}} = E_{\text{zugef.}} \cdot 0.85$$

$$0.85 \cdot 35 \text{ MJ} = E = c_{\text{Wasser}} \cdot m_{\text{Wasser}} \cdot \Delta T$$

$$29.75 \cdot 10^6 \text{ J} = c_W \cdot m_W \cdot \Delta T$$

$$m_{\text{Wasser}} = \frac{29.75 \cdot 10^6 \text{ Joule}}{c_W \cdot \Delta T}$$

$$= \frac{29.75 \cdot 10^6 \text{ J}}{4182 \frac{\text{J}}{\text{kg} \cdot \text{K}} \cdot (70^\circ\text{C} - 5^\circ\text{C})}$$

$$= \frac{29.75 \cdot 10^6 \text{ J}}{4182 \frac{\text{J}}{\text{kg} \cdot \text{K}} \cdot 65 \text{ K}} \approx \underline{\underline{109.44 \text{ L}}}$$



$$\textcircled{3} \left. \begin{array}{l} m_M = 0.3 \text{ kg}, T_M = 3^\circ\text{C} \\ m_{\text{Dampf}} = 28.5 \text{ g} = 0.0285 \text{ kg} \\ T_{\text{Dampf}} = 150^\circ\text{C} \end{array} \right\} T = \text{resultierende Mischtemp.}$$

~~$m_M \cdot c_W$~~

$$c_{\text{Wasser}} \cdot m_M \cdot (T - 3^\circ\text{C}) = c_{\text{Dampf}} \cdot m_D \cdot 50 \text{ K} + L_v \cdot m_D + c_W \cdot m_D \cdot (100^\circ\text{C} - T)$$

$$c_W \cdot m_M T - c_W m_M \cdot 3 \text{ K} = c_D \cdot m_D \cdot 50 \text{ K} + L_v \cdot m_D + c_W m_D \cdot 100 \text{ K} - c_W m_D \cdot T$$

$$T(c_W m_M + c_W m_D) = c_W m_M \cdot 3 \text{ K} + c_D \cdot m_D \cdot 50 \text{ K} + L_v \cdot m_D + c_W m_D \cdot 100 \text{ K}$$

$$T = \frac{c_W m_M \cdot 3 \text{ K} + c_D \cdot m_D \cdot 50 \text{ K} + L_v \cdot m_D + c_W m_D \cdot 100 \text{ K}}{c_W m_M + c_W m_D}$$

$$\underline{\underline{T \approx 60.15^\circ\text{C}}}$$

$$\begin{aligned} \text{Dampf } 150^\circ\text{C} \rightarrow 100^\circ\text{C}: Q_1 &= m_D \cdot c_D \cdot 50 \text{ K} \\ &= 0.0285 \cdot 1863 \cdot 50 \\ &= 2'654.775 \text{ Joule} \end{aligned}$$

$$\begin{aligned} \text{Phasenwechsel Dampf-Wasser}: Q_2 &= L_v \cdot m_D \\ &= 64'296 \text{ Joule} \end{aligned}$$

$$Q_1 + Q_2 = 66'950.775 \text{ J.}$$

$$T = \frac{3763.8 + 2654.775 + 64296 + 11918.7}{1254.6 + 119.187} = \frac{82633.275}{1373.787}$$



④

$$p = 1 \text{ bar}, T = 25^\circ \text{C} = 298 \text{ K}$$

$$\rho = 80.728 \text{ g/m}^3 = 0.080728 \text{ kg/m}^3$$

$$\rho = \frac{pM}{RT} \Rightarrow M = \frac{\rho \cdot R \cdot T}{p} \approx 0.002 \text{ kg/mol}$$

$2 \text{ g pro Mol} \Rightarrow \text{H}_2 \text{ (Wasserstoffgas)}$

⑤

$$1: p = 1.9 \text{ atü} = 2.9 \text{ atm}, T = 8^\circ \text{C} = 281 \text{ K}$$

$$2: p = 2.2 \text{ atü} = 3.2 \text{ atm}, T = ?$$

$$V_1 = V_2, n_1 = n_2 \Rightarrow \frac{p_1}{p_2} = \frac{T_1}{T_2}$$

$$\Rightarrow T_2 = T_1 \cdot \frac{p_2}{p_1}$$

$$T_2 = 281 \text{ K} \cdot \frac{3.2 \text{ atm}}{2.9 \text{ atm}} = 281 \text{ K} \cdot \frac{3.2}{2.9}$$

$$= 310.07 \text{ K} \approx \underline{\underline{37.07^\circ \text{C}}}$$

⑥

$$1 \text{ Mol H}_2\text{O}: M_{\text{H}_2\text{O}} = 18 \text{ g/mol}$$

$$pV = n \cdot R \cdot T; \quad p = 1 \text{ atm}, n = 1$$

$$T = 373 \text{ K}$$

$$\Rightarrow V = \frac{nRT}{p} \approx 3.061 \cdot 10^{-2} \text{ m}^3$$

$$= 30.61 \text{ Liter}$$

$$1 \text{ Mol flüssig: } V_1 = 18 \text{ cm}^3 = 0.018 \text{ L}$$

$$\text{als gasförmig: } V_2 = 30.61 \text{ L}$$

$$\frac{V_2}{V_1} = \frac{30.61}{0.018} \approx 1700\text{-mal größer!}$$



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KGG:

$$F_{\text{Auftrieb}} = F_G + F_{G, \text{Helium}}$$

$$\rho_{\text{Luft}} \cdot V \cdot g = mg + \rho_{\text{He}} \cdot V \cdot g$$

$$\rho_{\text{Luft}} \cdot V = m + \rho_{\text{He}} \cdot V$$

$$V(\rho_{\text{Luft}} - \rho_{\text{He}}) = m$$

$$V = \frac{m}{\rho_{\text{Luft}} - \rho_{\text{Helium}}}$$

a)  $\rho_1 = \frac{p_1 M}{R T_1}$  ;  $\rho_2 = \frac{p_2 M}{R T_2}$  ;  $p_1 = 101325 \text{ Pa}$ ,  $T_1 = 0^\circ\text{C}$

$$\frac{\rho_1}{\rho_2} = \frac{\frac{p_1 M}{R T_1}}{\frac{p_2 M}{R T_2}} = \frac{p_1 T_2}{p_2 T_1}$$

$$\frac{\rho_2}{\rho_1} = \frac{p_2 T_1}{p_1 T_2} \Rightarrow \rho_2 = \rho_1 \cdot \frac{p_2 T_1}{p_1 T_2}$$

Luft:  $\rho_1 = 1.293 \text{ kg/m}^3$ ,  $T_1 = 273 \text{ K}$ ,  $p_1 = 101325 \text{ Pa}$

$T_2 = 268 \text{ K}$ ,  $p_2 = 75000 \text{ Pa}$

$$\rho_2 = \rho_1 \frac{p_2 T_1}{p_1 T_2} \approx \underline{\underline{0.975 \text{ kg/m}^3}}$$

He:  $\rho_2 = \rho_1 \frac{p_2 T_1}{p_1 T_2} \approx \underline{\underline{0.135 \text{ kg/m}^3}}$

b)  $V = \frac{m}{\rho_{\text{Luft}} - \rho_{\text{He}}} = \frac{600 \text{ kg}}{(0.975 - 0.135) \text{ kg/m}^3} \approx \underline{\underline{714.3 \text{ m}^3}}$